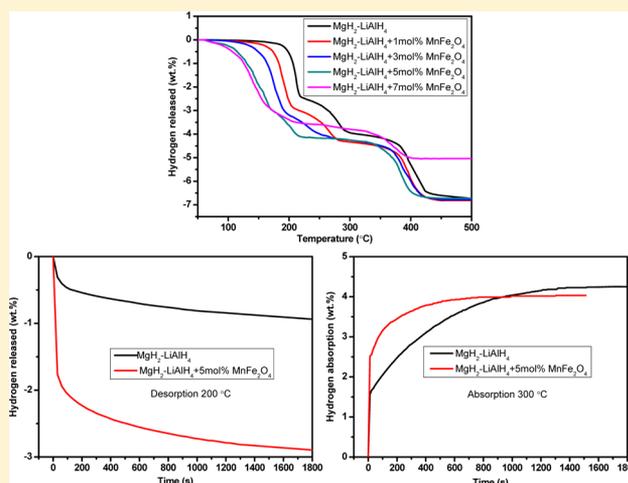


Improved Hydrogen Storage Performance of $\text{MgH}_2\text{-LiAlH}_4$ Composite by Addition of MnFe_2O_4

Qi Wan,[†] Ping Li,^{*,†} Ziliang Li,[†] Fuqiang Zhai,[‡] Xuanhui Qu,^{†,§} and Alex A. Volinsky^{||}[†]Institute for Advanced Materials and Technology, University of Science and Technology Beijing, Beijing 100083, China[‡]Departament Física Aplicada, EETAC, Universitat Politècnica de Catalunya-BarcelonaTech, 08860 Castelldefels, Spain[§]State Key Laboratory for Advanced Metals and Materials, University of Science and Technology Beijing, Beijing 100083, China^{||}Department of Mechanical Engineering, University of South Florida, Tampa, Florida 33620, United States

S Supporting Information

ABSTRACT: The catalytic effects of MnFe_2O_4 nanoparticles on the hydrogen storage properties of $\text{MgH}_2\text{-LiAlH}_4$, prepared by ball milling, are studied for the first time. The hydrogen storage properties and reaction mechanism are investigated by pressure–composition–temperature (PCT), differential scanning calorimetry (DSC), X-ray diffraction (XRD), and X-ray photoelectron spectroscopy (XPS). The nonisothermal desorption results show that $\text{MgH}_2\text{-LiAlH}_4 + 5$ mol % MnFe_2O_4 has a lower onset dehydrogenation temperature, 85, 50, and 40 °C lower than these of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample for each stage in the dehydrogenation process. The isothermal dehydrogenation kinetics and isothermal rehydrogenation kinetics results indicate that adding MnFe_2O_4 to $\text{MgH}_2\text{-LiAlH}_4$ could significantly enhance the absorption/desorption kinetics of $\text{MgH}_2\text{-LiAlH}_4$. From the differential scanning calorimetry and Kissinger analysis, the apparent activation energy of the 5 mol % MnFe_2O_4 -doped sample for the three decomposition stage is 55.8, 70.8, and 96.5 kJ/mol, resulting in a 45.7, 85.5, and 99.6 kJ/mol decrease, respectively, compared with the $\text{MgH}_2\text{-LiAlH}_4$ sample. These improvements are mainly attributed to in situ formed $\text{Fe}_{0.872}\text{O}$ phase and the amorphous Mn-containing phase during the dehydrogenation process, which act as the real catalyst in the $\text{MgH}_2\text{-LiAlH}_4 + 5$ mol % MnFe_2O_4 composite.



1. INTRODUCTION

Large gravimetric (≥ 5.5 wt %) and volumetric (≥ 40 g/L) densities are extremely eager for on-board hydrogen storage in fuel cell vehicles according to the U.S. DOE's 2015 target.¹ Magnesium hydride having high theoretical hydrogen storage capacity (7.6 wt %), abundant resources, and low cost can fully satisfy the demand of application.^{2–6} However, high desorption temperature (>400 °C) and relatively poor hydriding–dehydrogenation kinetics limit magnesium hydride practical applications.^{5–8} During the past decade researchers tried to address these challenges. Efforts included preparing nanoparticles by high-energy ball milling⁹ and adding catalysts, such as metals,^{5,9,10} C-containing species,^{11–14} metal oxides,^{15–18} metal halides,^{19,20} and other compounds.^{21–23} However, these endeavors could only strengthen its absorption/desorption kinetics properties. Thermodynamic performances of the magnesium hydride could hardly be changed.²⁴ From this view, researchers tried to destabilize MgH_2 using complex hydride with a high gravimetric density such as LiAlH_4 , which is an effective way to improve the hydrogen storage properties of MgH_2 and LiAlH_4 .^{24–29} However, the hydrogen storage

performances of the $\text{MgH}_2\text{-LiAlH}_4$ still need further improvement for practical application as a suitable hydrogen storage material, and the reaction mechanism and thermodynamics also require being demonstrated in more detail. Li et al.³⁰ and Zhai et al.³¹ reported that MnFe_2O_4 nanoparticles could remarkably improve the dehydrogenation properties of MgH_2 and LiAlH_4 alone. Therefore, it is reasonable to assume that MnFe_2O_4 would show great potential as a catalyst to promote $\text{MgH}_2\text{-LiAlH}_4$ system hydrogen storage performances. Motivated by the above findings, in this study, MnFe_2O_4 nanoparticles are employed as catalyst to study their effect on the hydrogen storage properties of the $\text{MgH}_2\text{-LiAlH}_4$ system by high-energy ball milling.

2. EXPERIMENTAL SECTION

Pure LiAlH_4 (hydrogen storage grade, $\geq 93\%$ purity) and MgH_2 (hydrogen storage grade) were purchased from Sigma Aldrich

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Co., and MnFe_2O_4 ($\geq 99.99\%$ purity, 20 nm particle size) was prepared by nitrate–citrate autocombustion methods. Details of the preparation procedure are given in our previous reports.^{30,32} All materials were used directly, with no further purification. All handling (including weighing and loading) was conducted in a glovebox filled with high-purity argon (99.999%) in order to prevent oxidation and moisture. Approximately 3 g of $\text{MgH}_2\text{-LiAlH}_4$ was mixed with different mole fractions (1, 3, 5, and 7 mol %) of MnFe_2O_4 nanoparticles and then ball milled for 30 min in a high-energy Spex Mill. MgH_2 and LiAlH_4 with a molar ratio of 1:1 will be referred to as $\text{MgH}_2\text{-LiAlH}_4$ for simplicity. $\text{MgH}_2\text{-LiAlH}_4$ was also prepared under the same conditions for comparison purposes. All samples were loaded into a 80 mL stainless steel pot in an argon-filled glovebox. ZrO_2 balls were added with a ball-to-powder weight ratio of 15:1. Samples were first ball milled for 10 min and then cooled down for 5 min after each cycle.

Hydrogen absorption and desorption properties of undoped and doped $\text{MgH}_2\text{-LiAlH}_4$ samples were measured using a pressure–composition–temperature (PCT) apparatus (Beijing Nonferrous Metal Research Institute, China). The highest pressure and temperature of the apparatus can be operated up to 10 MPa and 600 °C. The pressure of hydrogen in relation to volume was displayed by a pressure transducer. Experimental studies were done by a reactor that consisted of two parts: a heater and sample vessel. The former was used to connect with the pressure transducer and thermocouple. The reactor had a 1.5 cm outer diameter (o.d.), 0.5 cm wall, and 20 cm internal length, and it was loaded with the sample vessel (1 cm o.d., 0.1 cm wall, and 5 cm internal length). The reactor was heated with an air furnace. The mass of the sample used for measuring was kept at 0.3 g for each time, and the error range of temperature was controlled within ± 1 °C. From the value of hydrogen pressure change, the amount of hydrogen absorbed and desorbed could be obtained.^{33,34} For nonisothermal dehydrogenation, 0.5 g of the sample was loaded into the sample vessel in the glovebox and then heated up to 500 °C at a heating rate of 4 °C/min under 0.1 MPa atm pressure. The isothermal dehydrogenation behavior for undoped and doped samples was carried out at 200 and 300 °C under 0.1 MPa pressure, respectively. Following the first complete dehydrogenation, samples were subjected to rehydrogenation studies at 300 °C under 3 MPa of hydrogen pressure. The dehydrogenation/rehydrogenation amounts, calculated for all samples, were converted to pure $\text{MgH}_2\text{-LiAlH}_4$ with elimination of various impurities.

For analyzing the dehydrogenation performance and calculating the desorption activation energy of the undoped and doped $\text{MgH}_2\text{-LiAlH}_4$ sample by means of the Kissinger method, differential scanning calorimetry (DSC) was performed using NETZSCH STA 449C under a high-purity argon (99.999%) flow rate of 50 mL/min. About 5 mg of the sample was sealed into a 50 mL alumina crucible in the glovebox and then heated at different rates (4, 7, and 10 °C/min) from 50 to 500 °C.

Microstructural characterization of the samples after ball milling, after dehydrogenation, and after rehydrogenation was determined using the MXP21VAHF X-ray diffractometer with $\text{Cu K}\alpha$ radiation (40 kV, 200 mA) at room temperature. The 2θ angle was varied from 10° to 90° in 0.02° increments. X-ray photoelectron spectroscopy (XPS) was performed with the PHI-5300 spectrometer.

3. RESULTS AND DISCUSSION

Figure 1 presents the nonisothermal desorption curves of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped

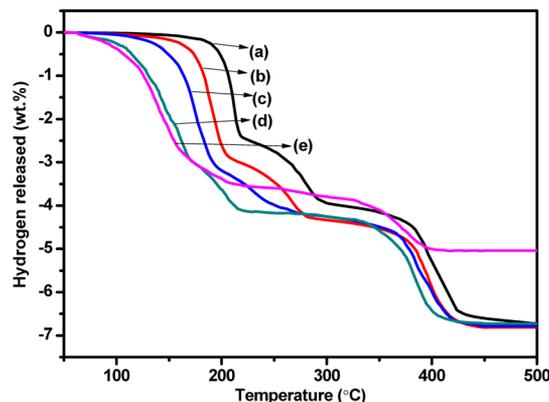


Figure 1. Thermal desorption curves of (a) ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with (b) 1, (c) 3, (d) 5, and (e) 7 mol % MnFe_2O_4 .

with 1, 3, 5, and 7 mol % MnFe_2O_4 nanoparticles. Desorption curves distinctly reveal that doping MnFe_2O_4 nanoparticles notably ameliorates $\text{MgH}_2\text{-LiAlH}_4$ dehydrogenation properties, resulting in a remarkable reduction of the desorption temperature. For the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample, three significant dehydrogenation stages are observed during the whole heating process: the first stage and second stage within the temperature ranges from 140 to 220 and 220 to 300 °C appear to be the first and second decomposition of LiAlH_4 . The third stage within the temperature ranging from 340 to 430 °C corresponds to the MgH_2 -relevant decomposition, agreeing well with previous literature,³⁵ and a total hydrogen release capacity of 6.71 wt % is obtained during these three decomposition processes.

While for the MnFe_2O_4 -doped samples, three stages of dehydrogenation are observed during the heating process. For the 1 mol % doped sample, the dehydrogenation process starts at 110 °C and terminates at 205 °C for the first decomposition stage and initiates at 205 and 325 °C and ends at 280 and 415 °C for the second and third decomposition steps, respectively. Further increase of additives amounts to 3 mol %; the onset dehydrogenation temperature reduces to 90, 195, and 310 °C for the three stages. Compared with ball-milled $\text{MgH}_2\text{-LiAlH}_4$, adding 1 and 3 mol % of MnFe_2O_4 causes a reduction in the onset desorption temperature of 30 and 50 °C for the first step, 15 and 25 °C for the second step, and 15 and 30 °C for the third step, respectively. During the three dehydrogenation processes, the sample with 1 mol % MnFe_2O_4 releases about 6.82 wt % hydrogen for three stages whereas 6.78 wt % hydrogen is desorbed for the 3 mol % doped sample, while for the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ + 5 mol % MnFe_2O_4 sample three stages of dehydrogenation occur during the heating process with a total hydrogen release amount of 6.74 wt %. The first stage proceeds in the temperature ranging from 55 to 170 °C, which is 85 and 50 °C lower than those of ball-milled $\text{MgH}_2\text{-LiAlH}_4$. The second stage takes place from 170 to 210 °C, resulting in 50 and 90 °C decreases, respectively. The third stage starts at 300 °C and is completed at 400 °C, causing reduction of 40 and 30 °C. With the amount of additive increasing to 7 mol %, the onset dehydrogenation temperature

decreases to 53, 160, and 270 °C, respectively, which indicates MnFe_2O_4 nanoparticles can significantly improve the dehydrogenation performance of the $\text{MgH}_2\text{-LiAlH}_4$ system. However, the desorption hydrogen content for the 7 mol % doped sample is only 5.04 wt % for the three steps, signifying a severe reduction in the hydrogen desorption capacity due to an excessive amount of MnFe_2O_4 nanoparticles. Therefore, the 5 mol % MnFe_2O_4 doped $\text{MgH}_2\text{-LiAlH}_4$ sample exhibits optimal dehydriding property, including the desorption temperature and hydrogen released capacity. Thus, utilizing the optimal 5 mol % MnFe_2O_4 -doped sample allows analyzing the MnFe_2O_4 catalytic mechanism in the following tests.

The dehydrogenation behavior of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 sample is further studied by DSC. Figure 2 shows the DSC

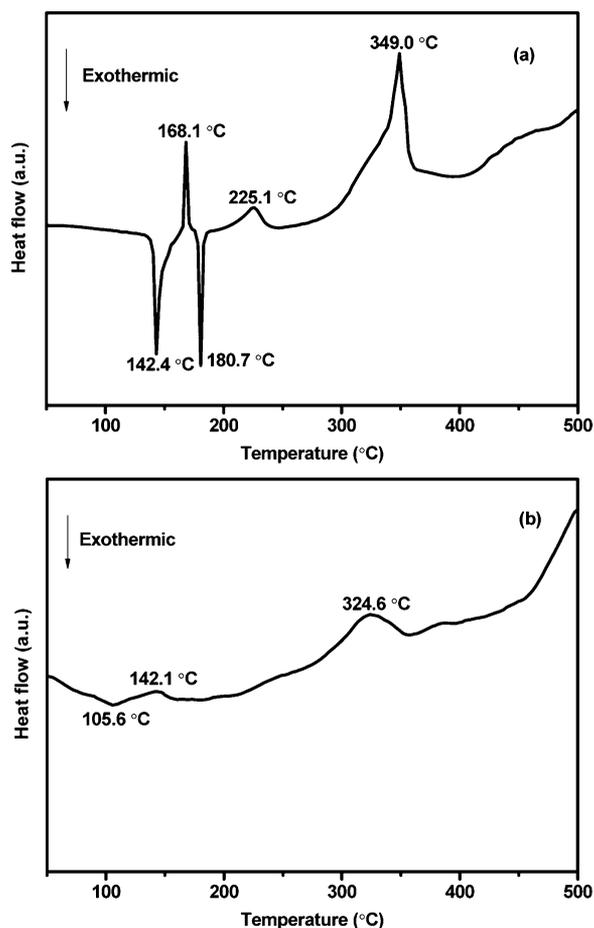
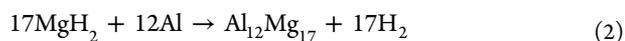
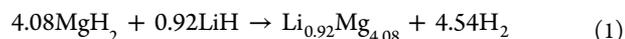


Figure 2. DSC profiles of (a) ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and (b) ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 within the 50–500 °C temperature range (10 °C/min heating rate).

curves of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample and ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 sample within 50–500 °C at a heating rate of 10 °C/min. As shown in Figure 2a, the DSC curve of the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample includes five distinct characteristics peaks, corresponding to two exothermic processes and three endothermic processes. The first exothermic peak turns up at 142.4 °C, corresponding to the interaction of LiAlH_4 with surface hydroxyl impurities,^{31,36–39} and the first endothermic peak appears at 168.1 °C arising from melting of LiAlH_4 .^{40–42} The second exothermic peak occurs at 180.7 °C due to decomposition of LiAlH_4 to

Li_3AlH_6 . The second and third endothermic peaks at 225.1 and 349.0 °C are both attributed to the MgH_2 -relevant decomposition.³⁵ Compared with the DSC plot of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample, the thermal decomposition behavior of $\text{MgH}_2\text{-LiAlH}_4 + 5$ mol % MnFe_2O_4 sample is markedly different, showing one exothermic peak and two broad endothermic peaks, in good agreement with reports.^{35,43} The exothermic peak occurs at 105.6 °C, and the first endothermic peak appears at 142.1 °C, which is attributed to decomposition of LiAlH_4 to Li_3AlH_6 and H_2 and decomposition of Li_3AlH_6 to LiH , Al , and H_2 , which is comparable with the three dehydrogenation steps in Figure 1 and in accord with literature,³⁵ but at a much lower temperature than the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample. Results demonstrate that LiAlH_4 starts to decompose at a little lower temperature before melting after adding MnFe_2O_4 catalyst, which agrees well with the results of ball-milled LiAlH_4 doped with 7 mol % MnFe_2O_4 reported by Zhai et al.³¹ The second endothermic peak at 324.6 °C corresponds to the MgH_2 -relevant decomposition, which is analogous to that of the $\text{MgH}_2\text{-LiAlH}_4$ sample. The remarkable decrease of the value of peak temperature in DSC curves indicates the dehydriding performances of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ are improved by MnFe_2O_4 nanoparticles. Nevertheless, the broad peak in the DSC curve of the $\text{MgH}_2\text{-LiAlH}_4 + 5$ mol % MnFe_2O_4 sample indicates a faster desorption kinetics performance at lower temperature. In addition, the decomposition temperature measured by DSC is higher than that tested by PCT. A similar phenomenon is also observed in the literature.^{35,38,39} These differences may result from the fact that the desorption measurement is carried out under different conditions for the samples tested with DSC (0.1 MPa argon, 10 °C/min) and PCT (0.1 MPa atm, 4 °C/min), resulting in different driving forces during the dehydrogenation process.

In order to analyze the mechanism in the dehydrogenation process, X-ray diffraction is performed on ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 . Figure 3 shows the XRD patterns of the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 after ball milling and after dehydrogenation at different temperatures. For the ball-milled sample, MgH_2 and LiAlH_4 phases are observed; a minor MnFe_2O_4 phase is detected. After the sample heats to 200 °C, LiAlH_4 phase disappears, new phases LiH and Al appear, while the MgH_2 phase still exists. Moreover, a small amount of $\text{Li}_{0.92}\text{Mg}_{4.08}$ phase and $\text{Fe}_{0.872}\text{O}$ phases are observed, indicating that hydrogen desorption from the doped sample below 200 °C is mainly attributed to dehydrogenation of LiAlH_4 with a small amount of MgH_2 -relevant decomposition. After heating to 300 °C, peaks of the MgH_2 and LiH/Al phases become weaker and a new $\text{Al}_{12}\text{Mg}_{17}$ phase is formed. Meanwhile, the amount of $\text{Li}_{0.92}\text{Mg}_{4.08}$ phase increases, and the $\text{Fe}_{0.872}\text{O}$ phase still exists. On further heating to 400 °C, the intensity of $\text{Li}_{0.92}\text{Mg}_{4.08}$ and $\text{Al}_{12}\text{Mg}_{17}$ phases becomes stronger, the peaks of MgH_2 , LiH , and Al phases disappear, and the $\text{Fe}_{0.872}\text{O}$ phase still can be observed, indicating that the hydrogen desorption in the temperature range of 200–400 °C is mainly due to reactions of Al and LiH with MgH_2 . According to the above results, the following reactions may take place during MgH_2 -relevant decomposition in the temperature range of 200–400 °C



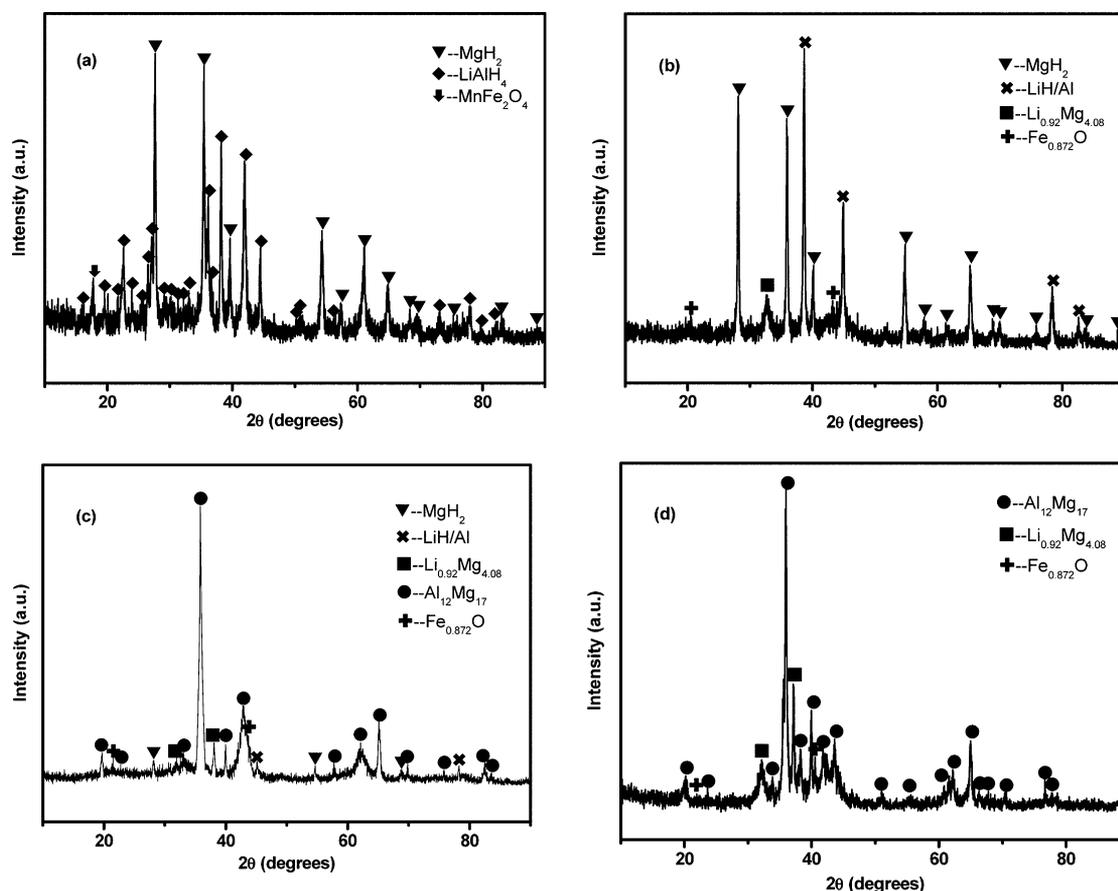


Figure 3. XRD patterns of the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 composite (a) after ball milling and after dehydrogenation at (b) 200, (c) 300, and (d) 400 °C.

Al–Mg and Li–Mg alloys are observed in this paper, which is accord with other literature.^{24,25,27,43} In addition, a new phase $\text{Fe}_{0.872}\text{O}$ is detected for the doped samples after decomposition at different temperatures, indicating that a reaction between LiAlH_4 and the MnFe_2O_4 catalyst happened during the dehydriding process. Nevertheless, no diffraction peaks of Mn-containing phase are observed due to the relatively lower amount or being in an amorphous phase.^{31,37,39}

The outstanding catalytic effect of MnFe_2O_4 nanoparticles on accelerating the dehydrogenation kinetics property of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample is further demonstrated by examination of isothermal desorption at constant temperature. For comparison, the desorption kinetics performance of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample is examined under the same conditions. Figures 4 and 5 show the dehydrogenation kinetics curves of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 samples at 200 and 300 °C under 0.1 MPa, respectively. It can be seen from Figure 4 that the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ system and the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 sample release 0.94 and 2.91 wt % hydrogen at 200 °C in 1800 s under 0.1 MPa pressure, respectively. Further increasing the temperature to 300 °C, the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 sample desorbs 4.09 wt % hydrogen within 15 s, which is much higher than that of $\text{MgH}_2\text{-LiAlH}_4$ sample (0.31 wt %) and TiF_3 -doped sample reported by Mao et al.³⁵ In contrast, about 1800 s is required for the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample to release 4.08 wt % hydrogen under the same conditions, which demonstrates MnFe_2O_4 superiority in improving $\text{MgH}_2\text{-LiAlH}_4$ dehydrogenation kinetics properties.

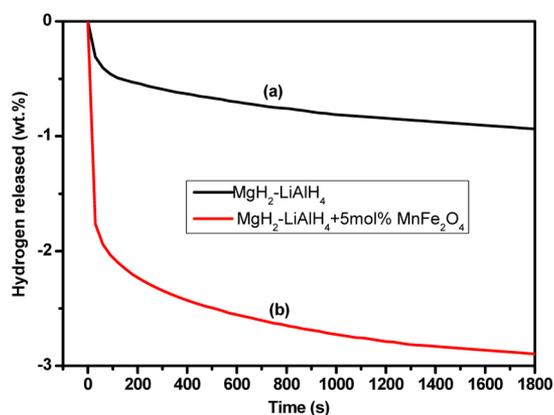


Figure 4. Isothermal desorption curves of (a) $\text{MgH}_2\text{-LiAlH}_4$ and (b) $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 samples at 200 °C.

Therefore, significant improvement of $\text{MgH}_2\text{-LiAlH}_4$ desorption kinetics can be obtained by adding MnFe_2O_4 nanopowders.

The desorption kinetics enhancement is connected with the energy barriers for hydrogen desorption. For investigating the dehydrogenation kinetics enhancement of the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \%$ MnFe_2O_4 sample in detail, DSC curves at different heating rates are measured to calculate the apparent activation energies of undoped and doped $\text{MgH}_2\text{-LiAlH}_4$ samples by the Kissinger method according to the following equation⁴⁴

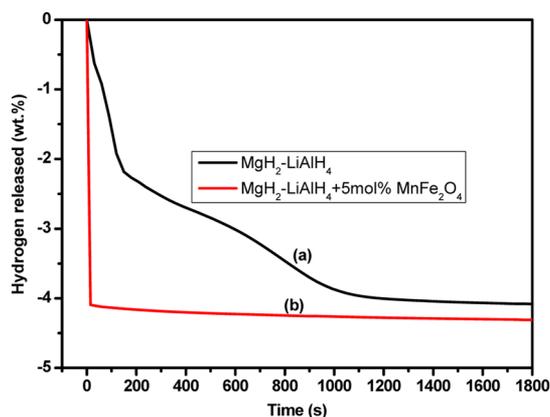


Figure 5. Isothermal desorption curves of (a) $\text{MgH}_2\text{-LiAlH}_4$ and (b) $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ samples at $300 \text{ }^\circ\text{C}$.

$$\frac{d \ln(\beta/T_p^2)}{d(1/T_p)} = -\frac{E_a}{R} \quad (3)$$

where β is the heating rate, R is the gas constant, and T_p is the value of the peak temperature in the DSC curve. Therefore, the apparent activation energy, E_a , can be obtained from the slope in a plot of $\ln(\beta/T_p^2)$ versus $1000/T_p$. The apparent activation energy of ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample is calculated to be 101.5, 156.3, and 196.1 kJ/mol, while these values decrease to 55.8, 70.8, and 96.5 kJ/mol for 5 mol % MnFe_2O_4 -doped $\text{MgH}_2\text{-LiAlH}_4$ sample. These results provide quantitative evidence for reduced desorption kinetics barriers during the dehydrogenating process, which indicates that MnFe_2O_4 nanoparticles can significantly improve the dehydrogenation performance of the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ system.

In order to investigate the reversibility of the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ and ball-milled $\text{MgH}_2\text{-LiAlH}_4$ doped with 5 mol % MnFe_2O_4 sample, rehydrogenation of the dehydrogenated sample is performed at $300 \text{ }^\circ\text{C}$ under 3 MPa of hydrogen pressure. Figure 6 presents the rehydrogenation kinetics curves of the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample and $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample at $300 \text{ }^\circ\text{C}$ under 3 MPa hydrogen pressure. It can be evidently seen from Figure 6 that the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample shows better rehydrogenation kinetics property than the $\text{MgH}_2\text{-LiAlH}_4$ sample. For the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample, 2.81

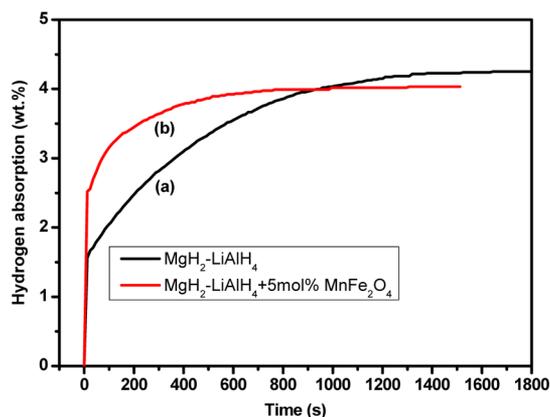


Figure 6. Isothermal rehydrogenation kinetics of (a) $\text{MgH}_2\text{-LiAlH}_4$ and (b) $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ samples at $300 \text{ }^\circ\text{C}$ under 3 MPa.

wt % hydrogen is absorbed within 300 s. However, a hydrogen absorption capacity of 3.64 wt % is reached within 300 s for the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample, which is higher than that of $\text{MgH}_2\text{-LiAlH}_4$ sample and TiF_3 -doped sample in other report.³⁵ These results demonstrate that the MnFe_2O_4 nanoparticles catalyst also remarkably improves the rehydrogenation kinetics performance of the $\text{MgH}_2\text{-LiAlH}_4$ sample.

To determine the rehydrogenation product, XRD analysis is carried out on the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample and $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample after rehydrogenation at $300 \text{ }^\circ\text{C}$ under 3 MPa hydrogen pressure, as presented in Figure 7. It is distinct that phases MgH_2 , LiH , and Al (Al and

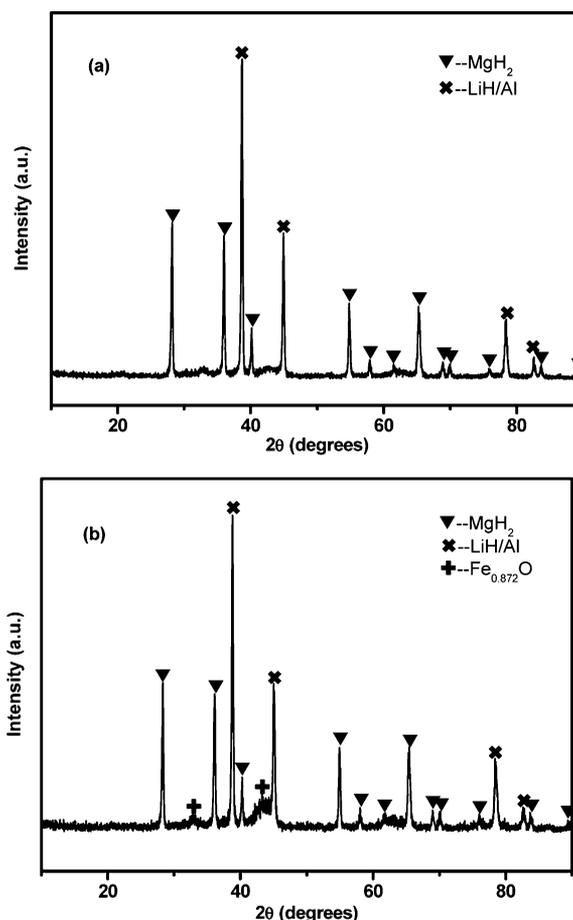
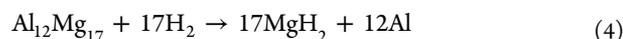


Figure 7. XRD patterns of (a) $\text{MgH}_2\text{-LiAlH}_4$ and (b) $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ samples after rehydrogenation at $300 \text{ }^\circ\text{C}$ under 3 MPa.

LiH peaks overlapping in the XRD patterns) are observed in both the undoped and the doped $\text{MgH}_2\text{-LiAlH}_4$ samples. However, no $\text{Al}_{12}\text{Mg}_{17}$ or $\text{Li}_{0.92}\text{Mg}_{4.08}$ alloy is detected in the rehydrogenated samples, indicating that full recovery of LiH and MgH_2 from $\text{Li}_{0.92}\text{Mg}_{4.08}$ and $\text{Al}_{12}\text{Mg}_{17}$ alloys has been achieved, as reported in the literature^{24,25,43} as follows



In addition, $\text{Fe}_{0.872}\text{O}$ phase is present in the rehydrogenated $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample, which is also detected in the dehydrogenated $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ sample. The formed $\text{Fe}_{0.872}\text{O}$ phase may be attributed

to reaction between LiAlH_4 and MnFe_2O_4 during the heating process, demonstrating that the MnFe_2O_4 nanoparticles in the ball-milled MgH_2 - LiAlH_4 doped with 5 mol % MnFe_2O_4 sample have a catalytic effect through formation of $\text{Fe}_{0.872}\text{O}$ phase and Mn-containing catalytic phase. Nevertheless, no phase containing Mn is observed after ball milling, after dehydrogenation, or after rehydrogenation due to the relatively lower amount or being in an amorphous phase. A study has been reported on the catalytic effect of MnFe_2O_4 on decomposition of LiAlH_4 , where the formed Fe oxide and the amorphous Mn-containing phase³¹ have a catalytic effect, which leads to improved hydrogen storage performances. The catalytic effect of Fe oxide and the Mn-containing species has also been proved to be important in improving the hydrogen storage properties of MgH_2 .³⁰ The dehydrogenation/hydrogenation properties are closely related with particle sizes and surface defects. The higher refinement is induced by adding MnFe_2O_4 nanoparticles. The refined particle size renders much shorter diffusion paths for hydrogen in the dehydrogenation/hydrogenation process. A decrease in particle size and crystallite size results in introducing a high surface defect density and creating more grain boundaries, which leads to surface activation and a larger surface area of MgH_2 and LiAlH_4 particles. Deformed and disordered surface regions are produced around finely dispersive Fe oxide and the Mn-containing species, exhibiting a lot of surface defects, which introduce a larger amount of reaction nucleation sites and hydrogen diffusion channels at the surface of the matrix for the dehydrogenation/hydrogenation process. The higher surface defect density and grain boundaries introduced by the dispersive Fe oxide and Mn-containing species improve the hydrogen storage properties. On the basis of the results reported above and the experimental results it can be concluded that the MnFe_2O_4 nanoparticles in the ball-milled MgH_2 - LiAlH_4 doped with 5 mol % MnFe_2O_4 sample play a catalytic effect through formation of $\text{Fe}_{0.872}\text{O}$ and the amorphous Mn-containing catalytic species, which may accelerate interaction of MgH_2 and LiAlH_4 and thus promote the hydrogen storage properties of the MgH_2 - LiAlH_4 sample.

To further analyze the nature of the Mn and Fe species after the ball milling, dehydrogenation, and rehydrogenation process, chemical characterization of Fe and Mn has been investigated by XPS in ball-milled, dehydrogenation, and rehydrogenation MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 samples. Figure 8 shows the XPS narrow scan spectra of Fe 2p for ball-milled, dehydrogenation, and rehydrogenation samples. The photoemission spectra of Fe 2p for ball-milled, dehydrogenation, and rehydrogenation samples all lie at 707.00 eV, corresponding to $\text{Fe}_{0.872}\text{O}_2$.³⁰ Figure 9 shows the XPS narrow scan spectra of Mn 2p for ball-milled, dehydrogenation, and rehydrogenation samples. The photoemission spectra of Mn 2p for ball-milled, dehydrogenation, and rehydrogenation samples all are located at 652.9 eV, corresponding to MnO_x/Mn_2 .³⁰ XPS results further demonstrate that MnFe_2O_4 can notably improve the dehydrogenation/rehydrogenation hydrogen properties of the MgH_2 - LiAlH_4 system by formation of $\text{Fe}_{0.872}\text{O}$ and the amorphous Mn-containing catalytic species.

4. CONCLUSION

The hydrogen storage properties of MgH_2 - LiAlH_4 are effectively improved by adding MnFe_2O_4 nanoparticles. Non-isothermal desorption measurement results show that the onset desorption temperature of the ball-milled MgH_2 - LiAlH_4 -

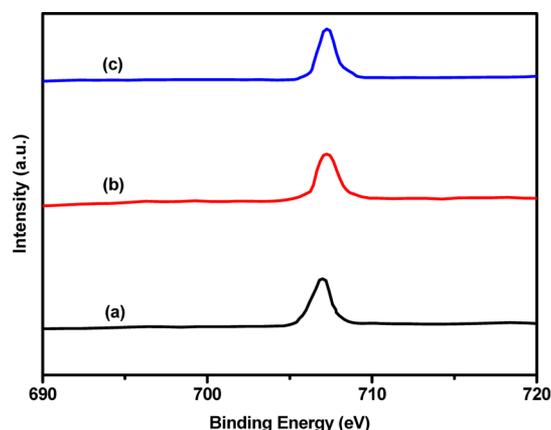


Figure 8. Narrow scan Fe 2p XPS of MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 (a) after ball milling, (b) after complete dehydrogenation, and (c) after rehydrogenation.

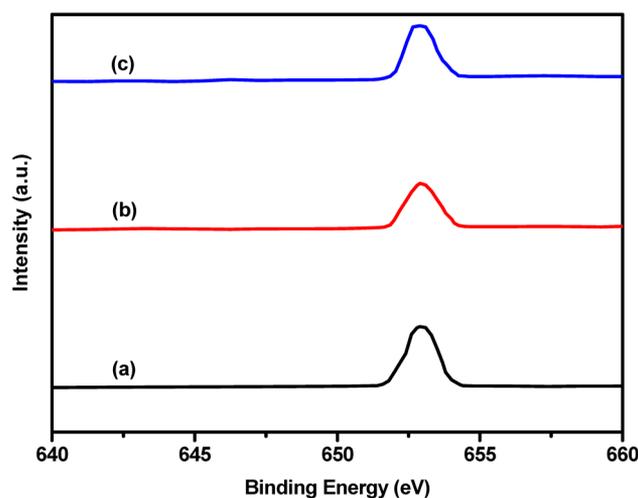


Figure 9. Narrow scan Mn 2p XPS of MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 (a) after ball milling, (b) after complete dehydrogenation, and (c) after rehydrogenation.

doped with 5 mol % MnFe_2O_4 is 55, 170, and 300 °C for the three steps, releasing 6.74 wt % hydrogen, resulting in a 85, 50, and 40 °C decrease, respectively, compared with the ball-milled MgH_2 - LiAlH_4 sample. Isothermal dehydrating kinetics shows that the ball-milled MgH_2 - LiAlH_4 system and MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 sample release 0.94 and 2.91 wt % hydrogen at 200 °C in 1800 s under 0.1 MPa pressure, respectively. On further increasing the temperature to 300 °C, the MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 sample releases 4.09 wt % hydrogen within 15 s while the ball-milled MgH_2 - LiAlH_4 sample only releases 0.31 wt % hydrogen under the same conditions, which demonstrates the MnFe_2O_4 nanoparticles can remarkably improve the dehydrogenation kinetics of MgH_2 - LiAlH_4 . Rehydrogenation kinetics measurement results show that 2.81 wt % hydrogen is absorbed at 300 °C within 300 s under a hydrogen pressure of 3 MPa for the ball-milled MgH_2 - LiAlH_4 sample. However, a hydrogen absorption capacity of 3.64 wt % is reached under the same conditions for the MgH_2 - LiAlH_4 + 5 mol % MnFe_2O_4 composite, which indicates the MnFe_2O_4 nanoparticles also remarkably improve the rehydrogenation kinetics performance of MgH_2 - LiAlH_4 . From differential scanning calorimetry and Kissinger analysis, the apparent activation energy of the 5 mol % MnFe_2O_4 -doped

sample for the three decomposition stages is 55.8, 70.8, and 96.5 kJ/mol, resulting in a 45.7, 85.5, and 99.6 kJ/mol reduction, respectively, compared with the ball-milled $\text{MgH}_2\text{-LiAlH}_4$ sample. The high catalytic activity of MnFe_2O_4 is associated with in situ formation of the Fe oxide phase and the amorphous Mn-containing phase from MnFe_2O_4 and LiAlH_4 during the dehydrogenation process. Therefore, the formed $\text{Fe}_{0.872}\text{O}$ phase and the amorphous Mn-containing phase act as real catalysts, which ameliorates the hydrogen storage properties of the $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ composite.

■ ASSOCIATED CONTENT

Supporting Information

DSC curves of as-milled $\text{MgH}_2\text{-LiAlH}_4$ and $\text{MgH}_2\text{-LiAlH}_4 + 5 \text{ mol } \% \text{ MnFe}_2\text{O}_4$ at heating rates of 4, 7, and 10 °C/min. This material is available free of charge via the Internet at <http://pubs.acs.org>.

■ AUTHOR INFORMATION

Corresponding Author

*Phone: +86-10-82377286. Fax: +86-10-62334311. E-mail: ustbliping@126.com.

Notes

The authors declare no competing financial interest.

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